

LINEAR STABILITY CONTINUED -

CAPILLARY INSTABILITY OF A CYLINDRICAL JET

THIS ANALYSIS WILL EXPLAIN AND QUANTIFY THE BREAK-UP OF A LIQUID JET, E.G., SEEN WHEN A THIN STREAM OF WATER FLOWS LAMINARLY FROM A TAP.

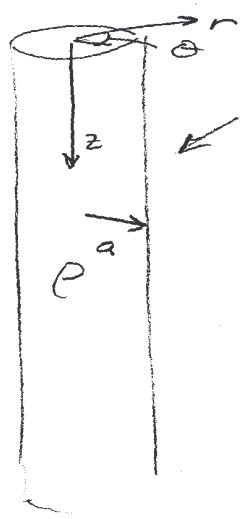
STRATEGY / KEY POINTS

- 1) CALCULATE OR GUESS BASIC STATE - (MUST SATISFY MOMENTUM & CONTINUITY AND APPROPRIATE BOUNDARY CONDITIONS ON BASIC FLOW)
- 2) STATE GOVERNING EQNS (MOMENTUM & CONTIN) AND BOUNDARY CONDITIONS
- 3) ASSUME PERTURBATIONS TO THE BASIC FLOW ARE OF NORMAL MODE VARIETY
- 4) LINEARIZE GOVERNING EQNS AND BOUNDARY CONDITIONS. THIS IS PERMISSIBLE (LIMITING) SINCE WE ARE FOCUSING[^] ATTENTION ON INITIAL, LOW AMPLITUDE PERTURBATIONS TO THE BASIC FLOW.

5) ATTEMPT TO SOLVE LINEARIZED SYSTEM OF EQNS. IN ORDER TO DETERMINE THE GROWTH RATE, $s = \sigma + i\omega$. THIS RELATIONSHIP (AN EIGENVALUE RELATIONSHIP) WILL DEPEND ON VARIOUS PROBLEM PARAMETERS (AS IN KELVIN-HOLMOLTZ); DETERMINING STABILITY OF BASIC FLOW TO NORMAL MODE DISTURBANCES BASED ON THE EIGENVALUE RELATIONSHIP DETERMINED.

BASIC FLOW

ASSUME (GUESS) THAT FLOW FIELD IN UNPERTURBED JET IS GIVEN BY



$\underline{u} = U_0 \hat{e}_z$
 undisturbed
 $a = \text{jet radius}$

$\underline{u} = U_0 \hat{e}_z$ where

$U_0 = \text{constant}$. ASSUME VISCOUS FORCES ARE NEGLIGIBLE WITHIN JET. IN REALITY, IF WE LOOK AT THE CASE WHERE

SAN WATER EXITS FROM A TAP, IT IS CLEAR THAT VORTICITY ($\nabla \times \underline{u}$) IS CREATED AT THE PERIPHERY OF THE LIQUID AS IT LEAVES THE TAP. AS DESCRIBED BY THE VORTICITY (LARGELY IN θ -DIRECTION) EQN., $\rho \frac{D\underline{w}}{Dt} = \mu \nabla^2 \underline{w}$, THIS VORTICITY WILL DIFFUSE INWARD TOWARD THE CENTER OF THE JET. WE CAN ESTIMATE HOW FAST THIS INWARDLY DIFFUSING VORTICITY WILL DIFFUSE TO THE CENTER BY ARGUING THAT RADIAL (INWARD) DIFFUSION (OF θ -VORTICITY) MUST BE COMPARABLE TO AXIAL ADVECTION (OF θ -VORTICITY). THUS

$$\underbrace{U_0 \frac{d w_\theta}{dz}}_{\text{axial advection of } \theta\text{-vorticity}} \approx \underbrace{\nu \frac{\partial^2 w_\theta}{\partial r^2}}_{\text{radial diffusion of } \theta\text{-vorticity}}$$

scaling terms $\Rightarrow \frac{U_0}{z} \approx \frac{\nu}{\delta^2}$

solving for $\delta(z)$ $\Rightarrow \delta \approx \sqrt{\frac{\nu z}{U_0}} = \frac{z}{Re_z^{1/2}}$

OR SETTING $\delta = a \Rightarrow z \approx \frac{a^2 U_0}{\nu}$

(4)

TYPICAL WATER
 THUS, FOR A ⁿJET OF RADIUS $a = 5 \text{ mm}$

TRAVELING AT ~~344~~ $U_0 = 1 \text{ m/s}$,

$$z \approx \frac{25(10^{-6})(1)}{10^{-7}} \approx 250 \text{ m}. \text{ IN OTHER WORDS,}$$

THE VORTICITY CREATED AT THE TIP WILL
 REMAIN CONFINED TO THIN CIRCUMFERENTIAL
 BOUNDARY LAYER -- WE CAN NEGLECT THE
 EFFECT OF VORTICITY (AND THUS VISCOSITY
IN OUR ANALYSIS).

CONSIDERING ASSUMED BASIC FLOW

$\underline{u} = U_0 \hat{e}_z$ IT IS EASILY CONFIRMED
 THAT MOMENTUM BDN AND CONTINUITY
 ARE SATISFIED BY THIS VELOCITY FIELD.

CONSISTENT W/ THE ASSUMPTION (WHICH
 HASN'T BEEN EXPLICITLY STATED) THAT
 THE LIQUID JET FLOWS IN A LOW
 DENSITY, LOW VISCOSITY FLUID (SUCH
 AS AIR), $\underline{u} = U_0 \hat{e}_z$ IMPLIES THAT THE
 SHEAR STRESS INDUCED BY THE SURROUNDING
 FLUID IS ZERO (SINCE $\frac{\partial u}{\partial r} = 0$).

IN REALITY, THIS IS NOT STRICTLY TRUE
 (SINCE, E.G., $\mu_{\text{air}} \neq 0$). HOWEVER, FOR PURPOSES
 OF OBTAINING A SIMPLE BASIC FLOW
 WHICH CAPTURES THE ACTUAL FLOW

⑤

WITHIN THE JET, THIS IS A REASONABLE APPROXIMATION. (AGAIN, OUR APPROXIMATIONS AND ASSUMPTIONS MUST EITHER BE RIGOROUSLY JUSTIFIED THROUGH CLEAR UNAVAILABLE PHYSICAL ARGUMENTS OR THROUGH EXPERIMENTS.)

④ NOTE, SINCE WE ARE ASSUMING $U_0 =$ CONSTANT, WE ARE IMPLICITLY ASSUMING THAT CHANGES IN GRAVITATIONAL POTENTIAL ENERGY ARE SMALL COMPARED TO THE JET'S CHARACTERISTIC KINETIC ENERGY. IN OTHER WORDS, USING BERNOULLI'S LAW (WHICH APPLIES TO INVISCID FLOW), WE CAN DETERMINE A CONDITION ON THE MAXIMUM ALLOWABLE JET LENGTH, Δz_{max} , OVER WHICH U IS ESSENTIALLY CONSTANT:

$$\frac{U_0^2}{2} + gz_1 = \frac{(U_0 + \Delta U)^2}{2} + gz_2$$

(NOTE P W/IN UNDISTURBED JET IS CONSTANT)

$$\begin{aligned} \Rightarrow z_1 - z_2 = \Delta z_{max} &= \frac{1}{2g} U_0^2 \left[1 + 2\left(\frac{\Delta U}{U_0}\right) + \left(\frac{\Delta U}{U_0}\right)^2 - 1 \right] \\ &= \frac{U_0^2}{2g} [2\epsilon + \epsilon^2] \quad \epsilon = \frac{\Delta U}{U_0} \end{aligned}$$

FOR $\epsilon \ll 1 \Rightarrow \epsilon \approx \frac{g \Delta z}{U_0^2} \ll 1 \Rightarrow \boxed{\Delta z \ll \frac{U_0^2}{g}}$

6

THUS, FOR A JET HAVING CHARACTERISTIC SPEED $u_0 = 1 \text{ m/s}$, $D \ll \sim 0.1 \text{ m} = 10 \text{ cm} \approx 4 \text{ in}$, BASED ON ATTACHED PHOTOS (SCALE IS IN UNITS OF CM) THIS CONDITION APPEARS TO BE WELL MET.

GOVERNING EQNS

(1) MOMENTUM $\boxed{\rho \frac{D\underline{u}}{Dt} = -\nabla P}$ (neglecting gravity)

(2) CONTIN $\boxed{\nabla \cdot \underline{u} = 0}$

KINEMATIC CONDITION (PARTICLES ON SURFACE OF JET REMAIN THERE);

$$r = F(z, \theta, t)$$

$$\Rightarrow \frac{dr}{dt} = F_{,z} \frac{dz}{dt} + F_{,\theta} \frac{d\theta}{dt} + F_{,t}$$

(3) $\Rightarrow \boxed{u = w F_{,z} + \frac{V F_{,\theta}}{r} + F_{,t}} \quad \text{on } r = F$

$u = r\text{-vel.}$

$v = \theta\text{-vel.}$

$w = z\text{-vel.}$

Note $v = r \frac{d\theta}{dt}$

(7)

NORMAL STRESS CONDITION AT JET/GAS INTERFACE

$$\sigma_{ij}^{(l)} n_i n_j - \sigma_{ij}^{(g)} n_i n_j = \gamma \nabla \cdot \underline{n}$$

$$p^{(l)} \delta_{ij} n_i n_j - p^{(g)} \delta_{ij} n_i n_j = "$$

(4)

$$\boxed{p^{(l)} - p^{(g)} = \gamma \nabla \cdot \underline{n}}$$

Recall that this is the Young-Laplace eqn. where $p^{(l)}$ is the liquid-side pressure, $p^{(g)}$ is the gas-side pressure, γ is the surface tension coefficient, \underline{n} is the outward unit normal to the jet, and $\nabla \cdot \underline{n}$ is the jet's curvature.

NOTE 1: SINCE WE'RE NEGLECTING VISCOSITY, THE ^{VISCOUS} TERMS IN THE CONSTITUTIVE RELN. FOR A NEWTONIAN FLUID ($\sigma_{ij} = -p\delta_{ij}$

+ $\mu(u_{i,j} + u_{j,i}) - \frac{2}{3}\mu \nabla \cdot \underline{u} \delta_{ij}$) ARE NEGLECTED.

NOTE 2: SINCE FLOW IS INVISCID, WE CANNOT IMPOSE A SHEAR STRESS B.C. ON THE JET-GAS INTERFACE (SINCE ORDER OF MOMENTUM BDN GOES

FROM 2 TO 1, i.e., HIGHEST ORDER DERIVATIVES ARE 1ST ORDER IN EQN. (1)).

NOTE 3: ALTHOUGH IT IS POSSIBLE TO USE BERNOULLI'S EQN TO RELATE $p(x)$ TO u (OR EQUIVALENTLY THE VELOCITY POTENTIAL Φ) WITHIN THE JET (AS WAS DONE IN ANALYZING THE KEVIN HELMHOLTZ INSTABILITY), THIS TURNS OUT TO BE UNNECESSARY IN THIS PROBLEM.

NOTE 4: IF WE NEGLECT SURFACE TENSION EFFECTS, i.e., ASSUME THAT $p(x) = p(y)$ IN (4), WE ESSENTIALLY RETURN TO THE KEVIN-HELMHOLTZ INSTABILITY PROBLEM. THE CONDITION IN EQN. (4) IS ^{CLEARLY CRITICAL} TO ANALYZING CAPILLARY INSTABILITY.

NOW SINCE u_0 IS CONSTANT, WE CAN SIMPLIFY ^{THE} ANALYSIS BY USING A FRAME OF REFERENCE ATTACHED TO THE MOVING JET, i.e., DO A GALILEAN TRANSFORMATION. SINCE THE FRAME TRANSCATES AT FIXED

(9)

VELOCITY (u_0), THE FORCES OPERATING IN THE LAB FRAME ARE IDENTICAL TO THOSE IN THE MOVING (BUT NON ACCELERATING) FRAME. THUS, LET THE BASIC STATE BE GIVEN BY

$$\underline{u} = \underline{0} \quad (5)$$

ALSO LET $\underline{p}(0) = \underline{0}$ (6) (EQUIV. TO REFERENCING $\underline{p}(0)$ TO AMBIENT \underline{p})
LINEARIZATION (NEGLECT PRODUCTS OF PERTURBATION QTY'S.)

$$\text{LET } \begin{cases} \underline{u} = \underline{u} + \underline{u}' \\ p = p + p' = p(0) + p'(0) \\ F = a + F' \end{cases} \quad (7)$$

WHERE PRIMED QTY'S ARE PERTURBATIONS ON THE BASIC STATE VARIABLES. (WE'LL SIMPLIFY NOTATION BY WRITING $p(0)$ AS p AND $p'(0)$ AS p' .)

NOW WRITE MOMENTUM EQN: AND LINEARIZE:

$$p \left(\underline{u}'_{,t} + u'_{ir} \underline{u}'_{,r} + \frac{v'_{i2}}{r} \underline{u}'_{,2} + w'_{i2} \underline{u}'_{,2} \right) = -\nabla(p + p')$$

$$\Rightarrow \underline{p} \underline{u}'_{,t} = -\nabla p' \quad (8)$$

NOTE, $p = p(0) = \rho \nabla \cdot \underline{u} = \frac{\rho}{a} = \text{CONSTANT}$.

(10)

CONTY.

$$\boxed{\nabla \cdot \underline{u}' = 0} \quad (9)$$

KINEMATIC CONDITION

$$u' = w'(a + F')_{,z} + \frac{v'}{r}(a + F')_{,\theta} + (a + F')_{,t}$$

$$\Rightarrow \boxed{u' = F'_{,t}} \quad \boxed{r = a} \quad (10)$$

NORMAL STRESS CONDITION

$$(P + P') = \delta \nabla \cdot \underline{n} \quad (11)$$

n:

FOR NON-AXISYMMETRIC DISTURBANCES, IT'S EASIEST TO USE A FORMULA FROM VECTOR CALCULUS. FOR A 3-D SURFACE

$$r = F(z, \theta, t)$$

LET

$$G(r, z, \theta, t) = r - F = 0$$

THEN

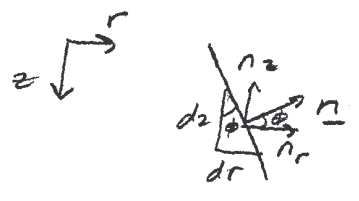
$$\underline{n} = \frac{\nabla G}{|\nabla G|} = \frac{\left(\hat{e}_r \frac{\partial}{\partial r} + \frac{\hat{e}_\theta}{r} \frac{\partial}{\partial \theta} + \hat{e}_z \frac{\partial}{\partial z} \right) (r - F)}{|\nabla G|}$$

$$\rightarrow \nabla G = \hat{e}_r - \frac{F_{10}}{r} \hat{e}_\theta - F_{12} \hat{e}_z$$

$$\Rightarrow |\nabla G| = \sqrt{\nabla G \cdot \nabla G} = \sqrt{1 + \left(\frac{F_{10}}{r}\right)^2 + F_{12}^2}$$

$$\Rightarrow \underline{n} = \frac{\hat{e}_r - \frac{F_{10}}{r} \hat{e}_\theta - F_{12} \hat{e}_z}{\sqrt{1 + \left(\frac{F_{10}}{r}\right)^2 + F_{12}^2}} \quad (12)$$

CHECK USING AXISYMMETRIC DISTURBANCE (WHERE $F_{10} = 0$):



$$\begin{aligned} n_r &= \cos \phi \\ &= \frac{dz}{dr \sqrt{1 + \left(\frac{dr}{dz}\right)^2}} = \frac{1}{\sqrt{1 + \left(\frac{dr}{dz}\right)^2}} \\ n_z &= -\sin \phi \\ &= \frac{-(dr/dz)}{\sqrt{1 + \left(\frac{dr}{dz}\right)^2}} \\ &= -\frac{F_{12}}{\sqrt{1 + F_{12}^2}} \end{aligned}$$

THUS, THIS IS CONSISTENT W/ (11). LIKEWISE, IN CASE WHERE JET IS PERFECTLY CYLINDRICAL, $r = a$; SO THAT $F_{12} = F_{10} = 0$ AND $\underline{n} = \hat{e}_r$.

NOW WE CAN CALCULATE $\nabla \cdot \underline{n}$:

(12)

SINCE JET SURFACE IS DESCRIBED BY $r = F(z, \theta, t)$, WE DON'T INCLUDE $\hat{e}_r \frac{\partial}{\partial r}$ IN THE DIVERGENCE OPERATOR. THUS,

$$\nabla \cdot \underline{n} = \left(\hat{e}_\theta \frac{\partial}{\partial \theta} + \hat{e}_z \frac{\partial}{\partial z} \right) \cdot \left(\frac{1}{N} \right) \left[\hat{e}_r - \frac{F_{1\theta}}{r} \hat{e}_\theta - F_{1z} \hat{e}_z \right]$$

WHERE $N = \left[1 + \frac{F_{1\theta}^2}{r^2} + F_{1z}^2 \right]^{1/2}$

$$\begin{aligned} \nabla \cdot \underline{n} &= \left(\frac{1}{N} \right) \left(\frac{1}{r} \right) - \frac{1}{r^2} \frac{\partial}{\partial \theta} \left(\frac{F_{1\theta}}{N} \right) - \frac{\partial}{\partial z} \left(\frac{F_{1z}}{N} \right) \\ &= \left(\frac{1}{N} \right) \left(\frac{1}{r} \right) - \frac{1}{r^2} \frac{F_{1\theta\theta}}{N} + \frac{1}{r} \frac{F_{1\theta}}{N^3} \left(\frac{F_{1\theta} F_{1\theta\theta}}{r^2} + F_{1z} F_{1z\theta} \right) \\ &\quad - \frac{F_{1z z}}{N} + \frac{F_{1z}}{N^3} \left(F_{1\theta} F_{1\theta z} + F_{1z} F_{1z z} \right) \end{aligned} \tag{13}$$

NOW LINEARIZE $\nabla \cdot \underline{n} :$

$$\begin{aligned} \frac{1}{N} &= \left[1 + \frac{(F'_{1\theta})^2}{(a+F')^2} + (F'_{1z})^2 \right]^{-1/2} \\ &= \left[1 + \frac{(F'_{1\theta})^2}{a^2} \left(1 - 2 \frac{F'}{a} \right) + (F'_{1z})^2 \right]^{-1/2} \end{aligned}$$

LET $H = H[F'_{1\theta}, F'_{1z}, F'] = H[A, B, C] = \frac{1}{N}$

$$\Rightarrow H = H(0,0,0) + \frac{\partial H}{\partial A} \Big|_{0,0,0} A + \frac{\partial H}{\partial B} B + \frac{\partial H}{\partial C} C$$

$$\Rightarrow \frac{1}{N} = 1 - \frac{1}{2} \left(\frac{1}{a^2} \right) (F'_{1\theta})^2 - \frac{1}{2} (F'_{1z})^2$$

LIKELIHOOD

$$\frac{1}{r} = \frac{1}{a+F'} = \frac{1}{a} \left(1 - \frac{F'}{a}\right)$$

NOW LINEARIZE TERMS IN (13):

$$\Rightarrow \frac{1}{N(r)} = \left(1 - \frac{F'}{a}\right)$$

$$- \frac{1}{r^2} \frac{F'_{100}}{N} = - \left(\frac{1}{a^2}\right) (1) (F'_{100})$$

$$- \frac{F'_{122}}{N} = - F'_{122}$$

$$\Rightarrow v \cdot \underline{n} = \frac{1}{a} - \left(\frac{F'}{a^2} + \frac{F'_{100}}{a^2} + F'_{122}\right)$$

\Rightarrow (11) BECOMES

$$P + P' = \gamma \left[\frac{1}{a} - \left(\frac{F'}{a^2} + \frac{F'_{100}}{a^2} + F'_{122}\right) \right]$$

BUT IN BASIC FLOW, THE NORMAL STRESS CONDITION YIELDS

$$P(r) - P^0 = P = \gamma v \cdot \underline{n} = \frac{\gamma}{a} \Rightarrow P = \frac{\gamma}{a}$$

THUS, LINEARIZED NORMAL STRESS CONDITION IS:

$$P' = -\gamma \left[\frac{F'}{a^2} + \frac{F'_{100}}{a^2} + F'_{122} \right] \quad (14)$$

$$\text{ON } r=a$$

(19)

THUS, FROM (8), (9), (10), AND (14) WE HAVE THE FOLLOWING LINEARIZED SET OF EQNS. THAT GOVERN THE JET'S STABILITY

$$\rho \underline{u}'_{,t} = -\nabla p' \quad (8)$$

$$\nabla \cdot \underline{u}' = 0 \quad (9)$$

$$\underline{u}' = \underline{F}'_{,t} \quad (r=a) \quad (10)$$

$$p' = -\gamma \left[\frac{F'_{,1}}{a^2} + \frac{F'_{100}}{a^2} + F'_{122} \right] \quad (r=a) \quad (14)$$

NOTE $\underline{u}' = r$ -COMP. OF PERTURBATION VELOCITY

NORMAL MODES - ASSUME PERTURBATIONS TO THE BASIC FLOW ARE OF NORMAL MODE FORM;

$$(15) \quad (\underline{u}', p', F') = (\underline{\hat{u}}(r), \hat{p}(r), \hat{F}) e^{st} e^{i(k_2 z + n\theta)}$$

NOTE AZIMUTHAL WAVE MODES MUST BE OF THE FORM $n\theta$ WHERE $n=0, 1, 2, 3, \dots$ IN ORDER FOR \underline{u}' , p' , AND F' AT θ TO BE IDENTICAL TO \underline{u}' , p' , AND F' AT $\theta + 2\pi$.

NOW TAKE DIVERGENCE OF (8) TO OBTAIN

$$-\rho \nabla(\underline{u}'_t) = -\rho (\nabla \cdot \underline{u}')_t = \boxed{\nabla^2 P' = 0} \quad (15)$$

US, (15) \rightarrow (16) \Rightarrow $\frac{d^2 \hat{P}}{dr^2} + \frac{1}{r} \frac{d\hat{P}}{dr} - \frac{\hat{P}}{r^2} n^2 - \hat{P} k^2 = 0$

$$\boxed{r^2 \hat{P}'' + r \hat{P}' - \hat{P}(n^2 + r^2 k^2) = 0} \quad (17)$$

THIS IS A
A MODIFIED BESSEL E.Q.N. OF ORDER n .

THE
SOLN IS GIVEN BY

$$\hat{P}(r) = a_1 I_n(kr) + b_1 K_n(kr) \quad (18)$$

(I_n = MODIFIED BESSEL FN OF FIRST KIND)
SINCE $K_n \rightarrow \infty$ AS $r \rightarrow 0$ THEN $b_1 = 0$

$$\Rightarrow \boxed{\hat{P}(r) = a_1 I_n(kr)} \quad (19)$$

NOW INTEGRATING (8) W.R.T. TIME YIELDS

$$\underline{u}'(r, z, \theta, t) - \underline{u}'(r, z, \theta, 0) = \frac{1}{\rho} \int_0^t \left[\frac{d\hat{P}}{dr} \hat{e}_r + \frac{1}{r} \hat{P} i n \hat{e}_\theta + \hat{P} i k \hat{e}_z \right] e^{i(kz + n\theta)} e^{st} dt$$

$$= -\frac{1}{\rho s} e^{i(kz + n\theta)} \left[\frac{d\hat{P}}{dr}, \frac{i n \hat{P}}{r}, i k \hat{P} \right] (e^{st} - 1)$$

SINCE

$$\text{BUT, } \underline{u}'(r, z, \theta, 0) = \underline{\hat{u}}(r) e^{i(kz + n\theta)}$$

$$\underline{u}'(r, z, \theta, t) = \underline{\hat{u}}(r) e^{i(kz + n\theta)} e^{st}$$

THEN

$$\hat{\underline{u}}(r) = -\frac{L}{\rho S} \left[\frac{d\hat{P}}{dr}, \frac{i n \hat{P}}{r}, i k \hat{P} \right] \quad (20)$$

OR USING (19)

$$(21) \quad \hat{\underline{u}}(r) = -\frac{a_1}{\rho S} \left[\underset{\substack{\uparrow \\ r\text{-comp}}}{k I_n'(kr)}, \underset{\substack{\uparrow \\ \theta\text{-comp}}}{\frac{i n}{r} I_n(kr)}, \underset{\substack{\uparrow \\ z\text{-comp}}}{i k I_n(kr)} \right]$$

NOW FROM (21) AND (10) WE GET

$$-\frac{a_1}{\rho S} k I_n'(ka) = S \hat{F}$$

$$\Rightarrow \hat{F} = -\frac{a_1}{\rho S^2} k I_n'(ka) \quad (22)$$

THUS, (14) YIELDS

$$\hat{P}(a) = \left[a_1 I_n(ka) = -S \hat{F} \left[\frac{L}{a^2} - \frac{n^2}{a^2} - k^2 \right] \right] \quad (23)$$

ELIMINATING a_1 & \hat{F} FROM (22) & (23)
YIELDS THE EIGENVALUE RELATIONSHIP
FOR THE GROWTH RATE S :

$$I_n(ka) = \frac{S k}{\rho S^2} I_n'(ka) \left[\frac{L}{a^2} - \frac{n^2}{a^2} - k^2 \right]$$

(17)

$$\Rightarrow \boxed{s^2 = \frac{\gamma K}{\rho a^2} \frac{I_n'(ka)}{I_n(ka)} [1 - n^2 - a^2 k^2]} \quad \begin{matrix} (*) \\ (*) \end{matrix} \quad (29)$$

LET $\beta = ka \stackrel{2\pi a/\lambda}{=}$. THEN (29) CAN BE REWRITTEN AS

$$\boxed{s^2 = \frac{\gamma \beta}{\rho a^3} \frac{I_n'(\beta)}{I_n(\beta)} [1 - n^2 - \beta^2]} \quad (30)$$

THE STABILITY CHARACTERISTICS OF THE CYLINDRICAL JET CAN ^{NOW} BE DETERMINED BY ANALYZING (30) (OR (29)). FIRST NOTE

THAT $\frac{I_n'(\beta)}{I_n(\beta)} > 0$ FOR ALL $\beta > 0$.

($\beta > 0$ SINCE $\beta = 0$ IMPLIES $\lambda \rightarrow \infty$.)

⊖ IN THE CASE WHERE $\boxed{n \neq 0}$, $1 - n^2 - \beta^2 < 0$.

THUS, $s^2 < 0$ SO THAT $s = \pm i\omega \Rightarrow$

ALL SUCH MODES ARE THUS STABLE ($\sigma = 0$).

NOTE THAT EACH MODE IN THIS CASE PERSISTS

AS A ^{STABLE} CYCLIC OSCILLATION OF FREQUENCY

$$\omega = \left(\frac{\gamma \beta}{\rho a^3} \frac{I_n'(\beta)}{I_n(\beta)} [n^2 + \beta^2 - 1] \right)^{1/2} \quad \text{THUS, } \begin{matrix} \text{FOR } n \neq 0 \\ \text{JET IS} \end{matrix}$$

STABLE TO ALL NON-AXISYMMETRIC MODES.

⊕ IN THE CASE WHERE $\boxed{n = 0}$, THE JET

IS UNSTABLE IF $1 - \beta^2 > 0$, I.E., IF

$$\boxed{0 < \beta < 1}.$$

IN THE CASE $n=0$, PERTURBATIONS HAVE NO θ -DEPENDENCE -- THESE ARE SYMMETRIC MODES. FOR A GIVEN JET RADIUS a , THE RANGE OF UNSTABLE WAVELENGTHS (FROM THE CONDITION $0 < \beta < 1$) SATISFIES

$$0 < \frac{2\pi a}{\lambda} < 1$$

OR

$$0 < 2\pi a < \lambda$$

THUS, ANY AXISYMMETRIC DISTURBANCE^(i.e., mode) HAVING A WAVELENGTH GREATER THAN THE JET'S CIRCUMFERENCE IS UNSTABLE.

IN CONTRAST, ANY AXISYMMETRIC MODE HAVING WAVELENGTH LESS THAN $2\pi a$ IS STABLE.

AS SHOWN ON THE ATTACHED GRAPH, COMPARING EXPERIMENTAL AND THEORETICAL CURVES OF

$$\frac{\sqrt{\rho a^3}}{\sqrt{\rho \beta}} = \frac{I_0'(B)}{I_0(B)} [1 - B^2] \text{ FROM (30)}$$

VS. β , THE LINEAR THEORY PREDICTS WELL OBSERVED VALUES OF $\frac{\sqrt{\rho a^3}}{\sqrt{\rho \beta}}$.

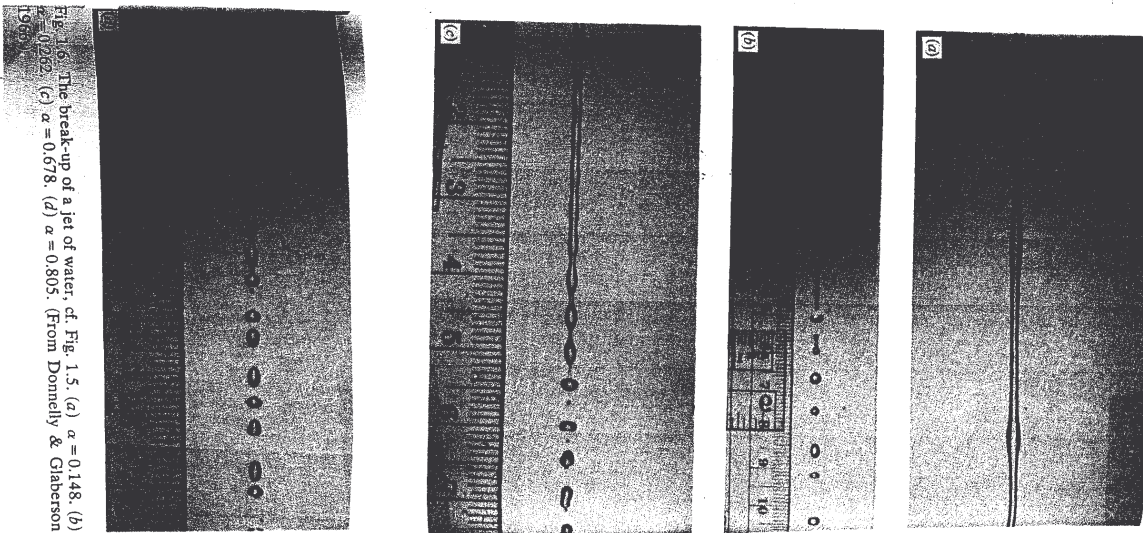


Fig. 1.6. The break-up of a jet of water: cf. Fig. 1.5. (a) $\alpha = 0.148$, (b) $\alpha = 0.252$, (c) $\alpha = 0.678$, (d) $\alpha = 0.805$. (From Donnelly & Glaberson 1966)

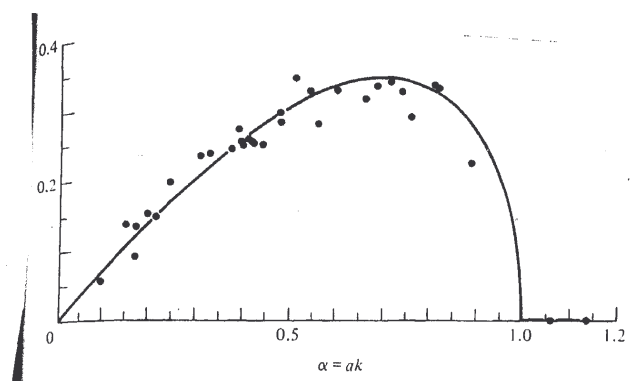


Fig. 1.5. The growth rates of unstable capillary modes of a uniform jet of fluid. (The solid line is based on the solution of equation (5.17) for an inviscid fluid by Chandrasekhar (1961), p.538 and the experimental points are from Donnelly & Glaberson (1966).)